Control Options	Off-gas				Capital	Operating		Total Annual	Cost Per /
	S	CFM	\$ SO2	SO2 tonnes per day	Cost 10 ⁶ ș	Cost 10 ⁶ ş	Amortization 10 ⁶ ș	Cost 10 ⁶ \$	cost Per tonne SO ₂ (2) removed \$
Single contact acid plant on strong gas stream									
- continuous gas only	27	000	12	346	17	1.5	2.5	4.0	33
- variable gas only	49	000	5-8	346	28	2.2	4.1	6.3	52
- continous gas & variable gas	36	000	6-12	346	22	1.8	3.1	4.9	40
Non-regenerative scrubbing of weak gas stream ⁽⁴⁾									•
- lime	400	000	1	430	40	17.4	5.7	23.1	154
- limestone	400	000	1	430	47	13.4	6.8	20.2	134
Regenerative scrubbing of weak gas stream(4)									
- MgO and acid plant	400	000	1	430	65	10.9	9.3	20.2	134
- Citrate and acid plant	400	000	1	430	58	7.9	8.3	16.2	108
Replacement of process pro- ducing weak gas stream with modern process (5)								-	
modern process (5) - existing old smelter process						26.0 ⁽⁶⁾		26.0	
(uncontrolled)				,		10			(-)
~- modern process	63	000	8	540	215	22.0(6)	30.9	52.9	115(7)

TABLE λ .4.2 Comparison of Cost of Abating SO₂ by Various Options⁽¹⁾

1. All costs are in 1981 U.S. dollars. Capital costs is amortized over 12.5 years at 10% interest.

2. Production is based on 350 operating days per year and assuming 100% control of SO₂.

 Figures are derived from "A Study of Sulfur Containment Technology in the Non-ferrous Metallurgical Industry", Economic and Technical Review Report EPS-3-AP-79-8, Air Pollution Control Directorate, Environment Canada, April 1980.

4. Non-regenerative and regenerative scrubbing of weak gas cost estimates are taken from the EPA data presented in the Appendices. The cost estimates for the regenerative scrubbing of weak gas stream also include a capital cost of \$20 million and an annual operating cost of \$6.8 million for a 660 tonnes per day sulfuric acid plant.

5. The cost estimates are for a copper smelter producing 100 000 tonnes per annum of copper. Modern processes are processes such as the INCO, Noranda and Mitsubishi processes.

6. The annual operating cost of a fully depreciated, existing reverb based smelter with no SO₂ controls is estimated to be about \$26 million. The operating cost of the modern processes is approximated at \$22 million.

7. The difference between the annual operating cost for the facility and the old facility are allocated to SO₂ control. The cost per tonne SO₂ fixed is computed assuming 100% SO₂ capture.