

C—DIRECT DERIVATIVES FROM THE ACETIC ACID.

The most important is acetone, a colorless liquid which is used as a solvent in aniline and several other branches of chemical manufacture, especially in the production of smokeless powder and other explosives. Acetone is obtained by separating acetic acid into three elements—acetone, carbonic acid and water. For this purpose the acetic acid is neutralized with lime, and the acetate thus formed is heated in a retort with a steam leading to a coal condenser. On account of the low boiling point of acetone (56°), this coil must be kept at a very low temperature in order to produce complete condensation. In the industrial process the acetate of lime is dried, finely pulverized and then put into the retort, where it is heated until the acetone has passed over, when the residuum is withdrawn and again used for making fresh acetate of lime, with which the operation is repeated. Acetone of 56° to 58° purity is now worth about 50 cents a kilogram (22.6 cents a pound), and, like acetate of lime, is a standard commercial product.

The next valuable derivative for acetic acid is wood alcohol or methyl alcohol, called in German "Holzgeist," a colorless, volatile and inflammable liquid, which boils at 66.3° C. and has a specific gravity of 0.800. It burns with a bluish flame of low illuminating power, dissolves resins, gums and essential oils and is extensively used in the manufacture of lacs and varnishes and for the denaturalization of spirits which are to be used for industrial purposes (in order to render them unfit for imbibation). The exports of wood alcohol from Germany in 1899 amounted to 6,703,620 pounds, valued at \$652,354.

Among the other useful products of wood distillation is oxalic acid, an important substance used in dyeing and cloth printing, which was formerly prepared by oxidizing sugar, but is now much more cheaply obtained from sawdust by the action of alkalies.

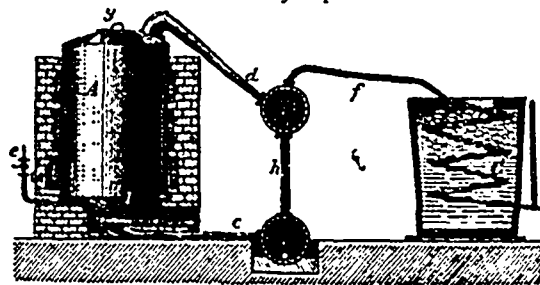
III.—APPARATUS FOR WOOD DISTILLATION.

Since the commencement of wood distillation as a practical industry nearly fifty years ago many changes and improvements have been made in the machinery employed, which for economical practice requires to be adapted to the kinds of wood to be worked, the quantity to be treated at each operation, and according to which of the distillates, tar or acid, is regarded of first importance. Wood is a bad conductor of heat, so that, in the construction of all retorts, the problem is to secure as prompt and as thorough a distribution of heat as possible throughout the mass, combined with such dimensions as will render the charging of the retort with wood and the withdrawing of the charcoal reasonably convenient. All plants for wood distillation combine substantially the features which are shown in the following model, which is a simple, upright retort, with a capacity of 8 cubic meters (about $2\frac{1}{2}$ cords) of wood.

In this figure, the retort A is made of ordinary or of galvanized boiler plate, set in brick masonry, with a spiral flue b, so that the fire introduced at the furnace a is drawn by the chimney draft round and round the outer shell of the retort, which is filled with wood, and the charcoal discharged through the manhole y. To quicken the heating of the charge to 100° C.—at which temperature the development of gases begins—superheated steam is turned in through the pipe c. The crude inflammable gases which are first generated are discharged downward into the fire through a pipe not shown in the drawing. As the heat increases the steam and gas pipes are closed and the distillates begin to pass over. The tar flows downward through the pipe c, the acid gases pass upward through

the beak d into the drum B, where the tarry vapors condense and are carried downward to the tar tank (lower B), which is kept cool by partial immersion in water. The pyroligenous acid gas, nearly freed from tarry impurities, passes on through f and the cold coil C, where it is condensed and pours out in the form of raw wood vinegar. These are the rudiments of the process.

In anticipation that the European process of making charcoal with recovery of the tar and acid products might have a practical interest for charcoal manufacturers in the United States, an engineer familiar with this industry has been consulted, and he has obtained from several German manufacturers of apparatus and fixtures for these purposes, estimates of the cost of equipment for a plant of the standard capacity, viz., 75 cubic meters (2,649 cubic feet) of wood daily. In practice it has been found most economical to set up the distillation plant as near as possible to where the wood is cut; in other words, at the point where all conditions of transportation for raw material and products are most favorable. The ordinary practice involves



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the distillation of hardwoods—beech or oak—and the recovery of charcoal, tar, raw wood vinegar and methyl alcohol. The charcoal, or first product, is ready for market upon being withdrawn from the retort. The tar is sent as raw material to chemical factories, where it is worked up as a separate industry. The methyl alcohol is also a commercial product and is usually sold in its crude state, but the wood vinegar is usually consumed on the spot for the production of acetate of lime, which, as already explained, is a convenient vehicle for recovering and transporting the pure acetic acid contained in the wood vinegar, which for this purpose is treated with ordinary limestone. Assuming, therefore, that a firm or company in the United States should wish to establish a modern German plant of this kind, and for that purpose to obtain the necessary machinery in this country, the calculation would be somewhat as follows.

Distilling apparatus, complete, without buildings, for treating 75 cubic meters of wood daily, would cost here 105,000 marks (\$24,090). If the capacity were increased to 100 cubic meters the cost of plant would be about 130,000 marks (\$30,940). If greater capacity is desired it would be advisable to duplicate the same apparatus instead of further increasing the size of the unit.

If beech wood is used, the raw vinegar obtained will be from 40 to 45 per cent. of the weight of the wood, and the vinegar should yield 9 to 12 per cent. of acetic acid. Assuming that this is to be recovered on the spot, a plant for the daily production of 1,200 kilograms (2,640 pounds) of acetate of lime would cost, exclusive of buildings, about 15,000 marks (\$3,570). This assumes that the raw pyroligenous acid is to be treated with ordinary limestone, a process which involves no technical difficulties. So far as can be ascertained, the apparatus for the industry involves few or no essential features which are covered by patents, so that a modern scientific plant, once established and its success demonstrated, could be duplicated to any extent which supply of material and the market for its products might require.

which would, until eliminated, injure the quality of the acetate.

Acetic acid is sufficiently powerful to expel carbonic acid in limestone, but the neutralization process causes thereby a strong effervescence, so that it must be accomplished in large, deep tanks in which the effervescing nature will not boil over. If instead of lime-burnt lime is used, the effervescence is greatly reduced; but in either case it is important that the amount of basic material (lime) be not in excess. In other words, it should be sufficient to neutralize the acetic acid—which it does first—and not enough to take up afterward the acid elements of the tar, which, being lighter than the acetate of lime, rise to the surface during the reaction and should be removed by skimming. The clarified solution is then evaporated in large shallow pans, yielding as a residuum crude acetate of lime. Overheating during the evaporation decomposes the acetate, so that a slow, steady and uniform heat is necessary, and for this purpose the off-gases from the retorts in which the wood is distilled are used whenever practicable. The residuum is a gray, odorless mass, containing about 75 per cent. of pure calcium acetate, and forms a standard article of commerce. It is purified by dissolving in water, passing through bone black, and concentrates by evaporation to a specific gravity of 1.16, when the salt crystallizes in small, odorless scales, which are principally used as material for the production of acetone.

Acetate of lime appears in commerce in three grades of purity, the highest of which is worth in large quantities 2.50 marks a kilogram (27 cents a pound); the medium, 1.60 marks (18 cents a pound), and the lowest 1.38 marks (15 cents a pound). Its commercial importance as a commercial product will be inferred from the fact that the exports of acetate of lime from Germany in 1898 were 539,300 kilograms; in 1899, 1,005,700 kilograms, and in 1900, 15,378,600 kilograms (3,395,000 pounds), of which last 1,382,140 pounds went to the United States.

When soda is used as the neutralizing base the product is acetate of soda, and the process throughout is in general similar to that when lime is employed. The acetate of soda has various uses, but its crystals disintegrate when exposed to the air, and for this and other reasons it is less important in Germany than acetate of lime. Both are, however, used as a means of extracting acetic acid from the raw wood vinegar, after which they are decomposed by various processes to obtain the crystallized acetic acid. When pure acid is to be obtained on a large scale the soda acetate is preferred, the acetic acid obtained from calcium acetate contains impurities which are difficult to separate. In other case, however, the acetate is decomposed by the action of a mineral acid sufficiently powerful to displace the acetic acid from combination with the base, by which process the former is isolated. Pure acetic acid is used for many purposes, amongst others making edible vinegar. When prepared for this purpose it must be carefully cleansed from empyreumatic impurities, which give it a disagreeable, smoky flavor. It is then made into table vinegar by dissolving in twenty times its volume of water.